Supplementary Information

Table SI1A: Capital equipment cost for all processing capacities

| EQUIPMEN | DPT | | | AW/AW S | JUSTIFICATIO | |
|--|----------|----------|--------------|--------------|--------------|--|
| COSTINGS | 200 kg/h | 600 kg/h | 1000 kg/h | 2000 kg/h | 2000 kg/h | N |
| Reactor | £45,000 | £135,000 | £225,000 | £450,000 | £450,000 | Derived from cost estimates for the equipment available at the Aston University demonstration plant (i.e. the 1 kg/h fast pyrolysis reactor) |
| Grinder | £100,000 | £100,000 | £100,000 | £100,000 | £100,000 | Estimate provided by commercial supplier |
| Sieve Machine | £25,000 | £25,000 | £25,000 | £25,000 | £25,000 | Estimate provided by commercial supplier |
| Wet Separator | | | | | £19,000 | Estimate provided by commercial supplier |
| Microturbin e (Dual Fuel) CHP 100 kW (@ £1280 per kW) | £128,000 | £128,000 | £128,000 | £128,000 | £128,000 | |
| Total Equipment Cost | £298,000 | £388,000 | £478,000 | £703,000 | £722,000 | |
| Total Equipment Cost (Exc dry pre- treatment) | £173,000 | £263,000 | £353,000 | £578,000 | £597,000 | |

Table SI1B: Staffing level for trommel fines fast pyrolysis energy system (Adapted from Yang et al., 2017)

| Capacity (kg h ⁻¹) | Day team | | Shift team | | Total (head) |
|--------------------------------|----------|------------|------------|----------|-----------------|
| | Manager | Technician | Supervisor | Operator | |
| 200 | 1 | 0.5 | 1 | 2 | 10.5 |
| 600 | 1 | 1 | 1 | 3 | 14 |
| 1000 | 1 | 1.5 | 1 | 3 | 14.5 |
| 2000 | 1 | 2 | 1 | 4 | 15.5 |

Table SI2: Energy production, total revenue and landfill costs from DPT trommel fines at different capacities

| CAPACITY | 200 kg/h | 600 kg/h | 1000 kg/h | 2000 kg/h |
|---|----------|----------|------------|------------|
| Feedstock (Tonnes per year) | 1600 | 4800 | 8000 | 16000 |
| Feedstock Calorific value (MJ/kg) | 13.80 | 13.80 | 13.80 | 13.80 |
| PT FP process conversion efficiency (η) | 41% | 41% | 41% | 41% |
| CHP efficiency | 60.0% | 60.0% | 60.0% | 60.0% |
| Conversion factor (to kWh) | 278 | 278 | 278 | 278 |
| Electricity selling price (£/unit) | £0.055 | £0.055 | £0.055 | £0.055 |
| Heat selling price (£/unit) | £0.0349 | £0.0349 | £0.0349 | £0.0349 |
| Gate fee (£/tonne) | £100 | £100 | £100 | £100 |
| Landfill disposal (£/tonne) | £115 | £115 | £115 | £115 |
| Available energy (GJ) | 22080 | 66240 | 110400 | 220800 |
| T Available energy (GJ) | 5432 | 16295 | 27158 | 54317 |
| Total Units produced | 1510007 | 4530021 | 7550035 | 15100070 |
| Income from heat (£) | £40,020 | £120,059 | £200,099 | £400,197 |
| Income from electricity (£) | £19,982 | £59,946 | £99,910 | £199,820 |
| Energy revenue (£) | £60,002 | £180,005 | £300,009 | £600,018 |
| Gate fee revenue (£) | £160,000 | £480,000 | £800,000 | £1,600,000 |
| Total revenue (£) | £220,002 | £660,005 | £1,100,009 | £2,200,018 |
| PT Land fill cost per year (£) | £184,000 | £552,000 | £920,000 | £1,840,000 |

DPT – Dry pre-treated trommel fines; FP – Fast pyrolysis

Table SI3: Capital and operating cost for Pyro-CHP of DPT feedstock at different processing capacities

| CAPACITY | 200 kg/h | 600 kg/h | 1000 kg/h | 2000 kg/h |
|-----------------------------|------------|------------|------------|------------|
| Total plant cost (TPC) (£) | £1,762,670 | £2,295,020 | £2,827,370 | £4,158,245 |
| Direct plant cost (DPC) (£) | £1,043,000 | £1,358,000 | £1,673,000 | £2,460,500 |
| Operating cost (£/year) | £651,513 | £1,002,957 | £1,214,360 | £1,731,200 |
| Maintenance (£/year) | £44,067 | £57,376 | £70,684 | £103,956 |
| Overheads (£/year) | £35,253 | £45,900 | £56,547 | £83,165 |
| Utility(£/year) | £82,054 | £246,162 | £410,269 | £820,539 |
| Labour cost (£/year) | £490,139 | £653,519 | £676,859 | £723,540 |

Table SI4: Energy production, total revenue and landfill costs for all three pre-treated feedstocks at 2000 kg/kg processing capacities

| SAMPLE | DPT | AW | AWS |
|--------------------------------------|------------|------------|------------|
| Feed (Tonnes per year) | 16000 | 16000 | 16000 |
| Feed Calorific value (MJ/kg) | 13.80 | 15.70 | 16.10 |
| FP process conversion efficiency (η) | 41% | 64% | 62% |
| CHP efficiency | 60.0% | 60.0% | 60.0% |
| Conversion factor (to kWh) | 278 | 278 | 278 |
| Electricity selling price (£/unit) | £0.055 | £0.055 | £0.055 |
| Heat selling price (£/unit) | £0.0349 | £0.0349 | £0.0349 |
| Gate fee (£/tonne) | £100 | £100 | £100 |
| Landfill disposal (£/tonne) | £115 | £115 | £115 |
| Available energy (GJ) | 220800 | 251200 | 257600 |
| T Available energy (GJ) | 54317 | 96461 | 95827 |
| Units produced | 15100070 | 26816102 | 26639962 |
| Income from heat (£) | £400,197 | £710,707 | £706,039 |
| Income from electricity (£) | £199,820 | £354,860 | £352,529 |
| Energy revenue (£) | £600,018 | £1,065,567 | £1,058,568 |
| Gate fee revenue (£) | £1,600,000 | £1,600,000 | £1,600,000 |
| Total revenue (£) | £2,200,018 | £2,665,567 | £2,658,568 |
| Land fill cost per year (£) | £1,840,000 | £1,840,000 | £1,840,000 |

DPT – Dry pre-treated trommel fines; AW – Agitated Washing; AWS – Agitated Washing with Surfactant (Decon Neutracon); FP – Fast pyrolysis

Table SI5: Capital and operating costs for all three pre-treated feedstocks, each processed at a capacity of 2000 kg/h.

| SAMPLE | DPT | AW | AWS |
|--|------------|------------|------------|
| Total plant cost (TPC) (£) | £4,158,245 | £4,270,630 | £4,270,630 |
| Direct plant cost (DPC) (£) | £2,460,500 | £2,527,000 | £2,527,000 |
| Operating cost (£/year) | £1,731,200 | £1,740,737 | £1,741,697 |
| Maintenance (£/year) | £103,956 | £106,766 | £106,766 |
| Overheads (£/year) | £83,165 | £85,413 | £85,413 |
| Utility - Electricity consumption (£/year) | £58,939 | £58,939 | £58,939 |
| Utility - Water usage (£/year) | £761,600 | £766,080 | £766,080 |
| Utility - Surfactant (£/year) | n/a | n/a | £960 |
| Labour cost (£/year) | £723,540 | £723,540 | £723,540 |

DPT – Dry pre-treated trommel fines; AW – Agitated Washing; AWS – Agitated Washing with Surfactant (Decon Neutracon)

Table SI6: Energy production, total revenue and landfill costs at 40% CHP efficiency for all three pre-treated feedstocks at 2000 kg/h processing capacities.

| SAMPLE | DPT | AW | AWS |
|--------------------------------------|------------|------------|------------|
| Feed (Tonnes per year) | 16000 | 16000 | 16000 |
| Feed Calorific value (MJ/kg) | 13.80 | 15.70 | 16.10 |
| FP process conversion efficiency (η) | 41% | 64% | 62% |
| CHP efficiency | 40% | 40% | 40% |
| Conversion factor (to kWh) | 278 | 278 | 278 |
| Electricity selling price (£/unit) | 0.055 | 0.055 | 0.055 |
| Heat selling price (£/unit) | 0.0349 | 0.0349 | 0.0349 |
| Gate fee (£/tonne) | £100 | £100 | £100 |
| Landfill disposal (£/tonne) | £115 | £115 | £115 |
| Available energy (GJ) | 220800 | 251200 | 257600 |
| T Available energy (GJ) | 36211 | 64307 | 63885 |
| Units produced | 10066714 | 17877402 | 17759974 |
| Income from heat (£) | £266,798 | £473,805 | £470,693 |
| Income from electrcity (£) | £133,214 | £236,573 | £235,019 |
| Energy revenue (£) | £400,012 | £710,378 | £705,712 |
| Gate fee revenue (£) | £1,600,000 | £1,600,000 | £1,600,000 |
| Total revenue (£) | £2,000,012 | £2,310,378 | £2,305,712 |
| Land fill cost per year (£) | £1,840,000 | £1,840,000 | £1,840,000 |

DPT – Dry pre-treated trommel fines; AW – Agitated Washing; AWS – Agitated Washing with Surfactant (Decon Neutracon); FP – Fast pyrolysis

Table SI7: Energy production, total revenue and landfill costs at 80% CHP efficiency for all three pre-treated feedstocks at 2000 kg/h processing capacities.

| SAMPLE | DPT | AW | AWS |
|--------------------------------------|------------|------------|------------|
| Feed (Tonnes per year) | 16000 | 16000 | 16000 |
| Feed Calorific value (MJ/kg) | 13.80 | 15.70 | 16.10 |
| FP process conversion efficiency (η) | 41% | 64% | 62% |
| CHP efficiency | 80% | 80% | 80% |
| Conversion factor (to kWh) | 278 | 278 | 278 |
| Electricity selling price (£/unit) | 0.055 | 0.055 | 0.055 |
| Heat selling price (£/unit) | 0.0349 | 0.0349 | 0.0349 |
| Gate fee (£/tonne) | £100 | £100 | £100 |
| Landfill disposal (£/tonne) | £115 | £115 | £115 |
| Available energy (GJ) | 220800 | 251200 | 257600 |
| T Available energy (GJ) | 72422 | 128614 | 127770 |
| Units produced | 20133427 | 35754803 | 35519949 |
| Income from heat (£) | £533,596 | £947,610 | £941,385 |
| Income from electricity (£) | £266,427 | £473,146 | £470,038 |
| Energy revenue (£) | £800,024 | £1,420,756 | £1,411,424 |
| Gate fee revenue (£) | £1,600,000 | £1,600,000 | £1,600,000 |
| Total revenue (£) | £2,400,024 | £3,020,756 | £3,011,424 |
| Land fill cost per year (£) | £1,840,000 | £1,840,000 | £1,840,000 |

DPT – Dry pre-treated trommel fines; AW – Agitated Washing; AWS – Agitated Washing with Surfactant (Decon Neutracon); FP – Fast pyrolysis

Table SI8: Capital and operating costs (excluding grinder and sieving unit operations) for all three feedstocks at 2000 kg/h processing capacities

| SAMPLE | DPT | AW | AWS |
|--|------------|------------|------------|
| Total plant cost (TPC) (£) | £3,418,870 | £3,531,255 | £3,531,255 |
| Direct plant cost (DPC) (£) | £2,023,000 | £2,089,500 | £2,089,500 |
| Operating cost (£/year) | £1,697,928 | £1,707,465 | £1,708,425 |
| Maintenance (£/year) | £85,472 | £88,281 | £88,281 |
| Overheads (£/year) | £68,377 | £70,625 | £70,625 |
| Utility - Electricity consumption (£/year) | £58,939 | £58,939 | £58,939 |
| Utility - Water usage (£/year) | £761,600 | £766,080 | £766,080 |
| Utility - Surfactant (£/year) | | | £960 |
| Labour cost (£/year) | £723,540 | £723,540 | £723,540 |

DPT – Dry pre-treated trommel fines; AW – Agitated Washing; AWS – Agitated Washing with Surfactant (Decon Neutracon)

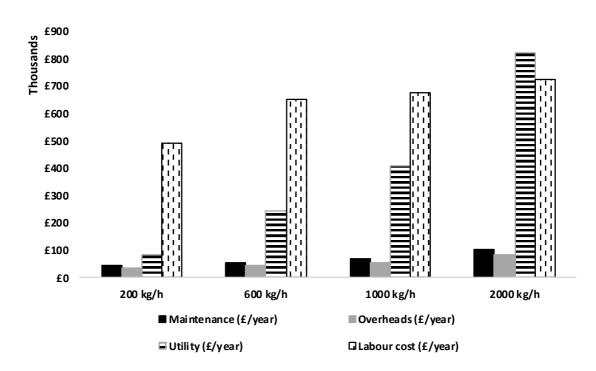


Figure SI1: Breakdown of operating cost for DPT trommel fines Pyro-CHP system at different capacities

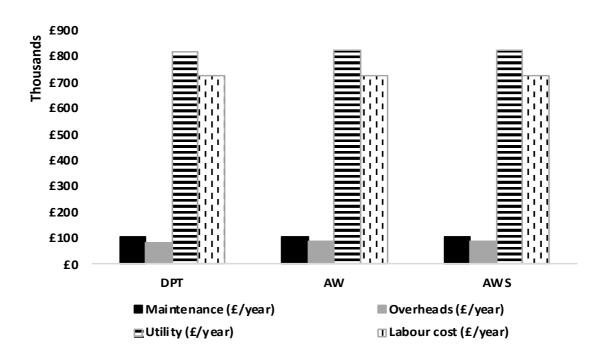


Figure SI2: Breakdown of operating cost for pyro-CHP systems using 2000 kg/h DPT, AW and AWS trommel fines feedstocks

DPT - fry pre-treated Trommel Fines; AW – Agitated Washing; AWS – Agitated Washing with Surfactant (Decon Neutracon)

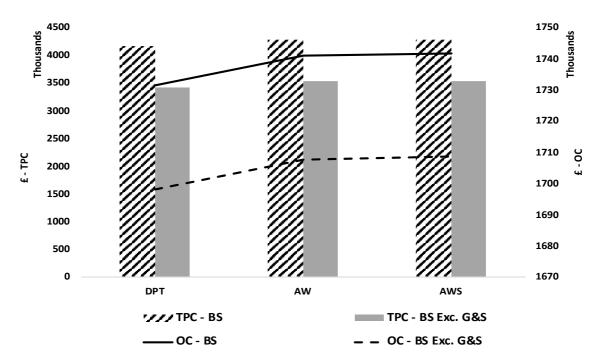


Figure SI3: Comparison of calculated capital investment and operating cost with (Base Scenario) and without grinding and sieving unit operations for pyro-CHP systems using DPT, AW and AWS trommel fines at 2000 kg/h capacities.

DPT - dry pre-treated Trommel Fines; AW – Agitated Washing; AWS – Agitated Washing with Surfactant (Decon Neutracon); TPC – Total Plant Cost; OC – Operating Cost; BS – Base Scenario; BS Exc. G&S – Base Scenario Excluding Grinder & Sieve