

Investigation of 2-butoxyethanol as biodiesel additive on fuel property and combustion characteristics of two neat biodiesels

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Abstract

Neat biodiesels are not preferred for use in the compression ignition (CI) engines due to their high viscosities and related operational difficulties. This study investigated the fuel properties and combustion characteristics when 2-butoxyethanol additive was mixed separately with waste cooking oil biodiesel (W100) and rapeseed oil biodiesel (R100). Compared to neat biodiesels, the viscosities (at 40 °C) of the W100 and R100 were reduced by 12.5% and 9.8% respectively, when they were blended separately with 15% 2-butoxyethanol. Four different samples such as W100, mixture of 85% W100 and 15% 2-Butoxyethanol (W85), R100, mixture of 85 % R100 and 15% 2-Butoxyethanol (R85) were tested in a multi-cylinder CI engine. The thermal efficiency of the W85 fuel was higher than fossil diesel by approximately 3.7%. Total combustion duration of the biodiesel-additive blends were shorter than neat biodiesels and fossil diesel. Biodiesel-additive blends provided approximately 6% higher in-cylinder peak pressures. At full load, W85 fuel gave up to 5.4% reduced NO_x emissions than neat biodiesel. The CO, HC and smoke emissions were decreased by up to 36%, 100% and 79% respectively. The study concluded that 2-butoxyethanol could effectively be used as biodiesel additive to improve fuel property; and to achieve better combustion and reduced pollution.

Keywords: biodiesel; CI engine; combustion; emission; fuel additive; performance.

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50 Abbreviations

51	aTDC	After top dead centre
52	BSFC	Brake specific fuel consumption
53	bTDC	Before top dead centre
54	BTE	Brake thermal efficiency
55	CA	Crank angle
56	CHO	Carbon, hydrogen and oxygen
57	CI	Compression ignition
58	DEF	Diesel exhaust fluid
59	DPF	Diesel particulate filter
60	EGR	Exhaust gas recirculation
61	FAME	Fatty acid methyl ester
62	FD	Fossil diesel
63	GCMS	Gas chromatography and mass spectrum
64	HVO	Hydrotreated vegetable oil
65	IC	Internal combustion
66	KOH	Potassium hydroxide
67	LHV	Lower heating value
68	OEM	Original equipment manufacturer
69	PAHs	Polycyclic aromatic hydrocarbons
70	PCDD/Fs	Polychlorinated dibenzo-p-dioxins and dibenzofurans
71	PM	Particulate matter
72	RO	Rapeseed oil
73	R100	Rapeseed oil biodiesel
74	R85	Rapeseed oil biodiesel 85% by volume and 2-Butoxyethanol 15% by volume
75	SCR	Selective catalytic reduction
76	ULSD	Ultra low sulphur diesel
77	WCO	Waste cooking oil
78	W100	Waste cooking oil biodiesel
79	W85	Waste cooking oil biodiesel 85% by volume and 2-Butoxyethanol 15% by volume

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84 1. Introduction

85

86 Due to high thermal efficiency and low weight-to-power ratio diesel engines are still popular and widely used in
87 many sectors. However, they consume huge quantities of fossil diesel fuel and emit harmful gas and soot
88 emissions which cause damage to the human health and environment [1–3]. The carbon soot from diesel engine
89 constitutes 73-83% of particulate matter (PM) [4]. The other pollutants in soot are: soluble organic fractions, ash
90 content, trace metals, sulphur compounds, and other substances like polycyclic aromatic hydrocarbons (PAHs)
91 [4,5]. Furthermore, polychlorinated dibenzo-p-dioxins and dibenzofurans (PCDD/Fs) are reported as pollutant
92 gas emissions from diesel engine [6,7]. The risk of respiratory, cardiovascular and lung cancer diseases are
93 enhanced when a human is exposed to PM emission. Selective catalytic reduction (SCR) and diesel particulate
94 filter (DPF) components are normally used to reduce the tail pipe NO_x and Particulate Matter (PM) emissions
95 respectively [8–10]. Other techniques such as exhaust gas recirculation (EGR), dual fuelling, water injection and
96 retardation of injection timing are also used to reduce the NO_x emission. However, adoption of these techniques
97 requires modifications on the engine component; hence, their applications are limited due to the additional
98 efforts and expenses involved.

99 Renewable alternative fuels could potentially be used in the internal combustion (IC) engines to replace fossil
100 based fuels and to reduce harmful gas emissions [11,12]. Biodiesels are considered as one of the most promising
101 alternative to fossil diesel due to better physico-chemical properties and life-cycle emission mitigation potential
102 [13,14]. Literature reported that in China, replacing petroleum diesel with waste cooking oil biodiesel would
103 decrease life cycle greenhouse gas emissions by up to 5.5x10⁶ tons of CO₂ equivalent [15]. Although, literature
104 agreed that biodiesel fuel significantly reduced the PM, HC, CO and CO₂ emissions, most researchers reported
105 that the use of 100% biodiesel fuels (B100) in the unmodified diesel engines gave higher NO_x emissions than

106 those obtained for pure fossil diesel [16,17]. This phenomenon is also known as ‘biodiesel NO_x penalty’ in the
107 literature [18]. Other technical issues associated with the neat biodiesel (B100) use are: (i) starting the engine in
108 cold weather, (ii) flow of biodiesel to injector due to higher viscosity, (iii) sticking and clogging of fuel injector
109 holes, fuel filters, and inlet/exhaust valves, and (iv) compatibility of fuel supply pipe materials with the biodiesel
110 [19–21]. To address these problems, Silva et al. investigated the effects of various alcohols used in
111 transesterification (biodiesel production) process on the fuel properties of Macauba oil biodiesel [22]. They
112 found that ethyl ester gave better cold filter plugging point property than methyl or isobutyl esters [22]. Another
113 approach is to blend biodiesel with another fuel. Literature reported that blending biodiesel with fossil fuels or
114 alcohols (and/or other additives) improved engine performance and reduced emissions [16,23]. Furthermore,
115 researchers found that blending neat biodiesel with additives gave lower NO_x and PM emissions than neat
116 biodiesel (B100) operation [24,25]. The most common alcohols used as biodiesel additives are ethanol and
117 methanol [26]. Datta and Mandal reported that blending palm stearin biodiesel with 15% methanol (or ethanol)
118 decreased the peak in-cylinder pressure with respect to the neat biodiesel [20]. They found that the NO_x
119 emissions were reduced by 19% and 30% due to methanol and ethanol addition respectively [20]. The smoke
120 opacity was decreased dramatically when the biodiesel-alcohol blend was used [20]. In another study, the
121 concentration of PM and PAHs emissions were investigated when 1-3% acetone and 1% isopropyl were added
122 in the waste cooking oil biodiesel [4]. The authors reported that the use of both additives helped to reduce the
123 PAH and PM emission by 24.1% and 53.2% respectively. Vedaraman et al. reported that NO_x emissions were
124 decreased when ethanol, methanol, diethyl ether and distilled water was added separately into fossil diesel-palm
125 oil biodiesel blend [27]. Addition of methanol and water reduced the NO_x emission by up to 2.7% and 7%
126 respectively [27]. However, they found out that the HC emission was increased with the distilled water addition
127 [27].

128 On the other hand, increase in the NO_x emissions were also observed by the researchers when additives such as
129 methanol, ethanol and butanol were added to neat biodiesel or diesel-biodiesel blends [28,29]. Yilmaz compared
130 the effects of ethanol and methanol addition in diesel-biodiesel blends in a two cylinder direct injection type
131 Kubota diesel generator set [28]. Blends containing 40% biodiesel-40% diesel-20% alcohol and 45% biodiesel-
132 45% diesel-10% alcohol, and neat fossil diesel were tested. The author reported that compared to fossil diesel,
133 the brake specific fuel consumption (BSFC) of ethanol and methanol blends were increased by up to 28.6% and
134 58.3% respectively. The author found that the methanol blends did not help to decrease the NO_x emissions.
135 Whereas, ethanol blends reduced the NO_x emissions by approximately 20% at mid-range loads [28]. Another
136 study conducted by Tosun et al. investigated the influences adding ethanol, methanol and butanol separately into
137 peanut oil biodiesel by testing these blends in a multi-cylinder direct injection type diesel engine [29]. They
138 reported that 20% blends of methanol, ethanol and butanol with peanut oil biodiesel enhanced the engine torque
139 output by about 1.2%, 3.4% and 6.1% respectively as compared to neat biodiesel operation. The CO emissions
140 of methanol, ethanol and butanol blends were decreased by 4.8%, 1.8% and 9.1% respectively. They observed
141 that the NO_x emissions were increased by 13.8%, 4.1% and 17.4% for 20% blends of methanol, ethanol and
142 butanol respectively [29]. Yasin et al. investigated the effects of 5% methanol addition on B20 blend with diesel
143 [25]. Methanol was mixed with the biodiesel-diesel blend using an ultrasonic agitator operated at 40 kHz
144 frequency. They found that the brake power for B20M5 fuel was decreased by approximately 7% and 10% than
145 B20 and neat diesel fuels respectively. The BSCF of the engine was increased by about 4-6% [25]. A reduction
146 of approximately 17-18% in CO and CO₂ emissions, and an increase of 13% in NO_x emission was reported
147 when the engine was fuelled with B20 M5 fuel [25]. In another study, Yilmaz investigated the effects of air
148 intake temperature when the engine was fuelled with 85% biodiesel-15% alcohol blends [26]. The author
149 reported that the CO and HC emissions were reduced by increasing the air intake temperatures and with the
150 increasing percentage of alcohol additives [26]. Sarikoc et al. tested butanol additive at 5% and 10% blend ratios
151 with 80% diesel - 20% waste cooking oil biodiesel blend [30]. They reported that the CO, CO₂, smoke opacity
152 and NO_x emissions were reduced by approximately 21%, 11%, 19% and 3% with 10% butanol addition [30].
153 However, HC emission was increased by approximately 32% as a result of worsened combustion efficiency
154 [30]. They also reported 16.17% reduction on thermal efficiency of the engine due to low LHV and cetane
155 number of the butanol [30]. The effect of n-butanol additive was also investigated along with the engine
156 modifications such as EGR, piston geometry, injection timing and injection pressure [31]. The authors found out
157 that toroidal piston was most suitable for n-butanol/diesel blends than biodiesel and diesel [31]. Zhang et al.
158 investigated the influence of n-butanol, n-octane and 2-ethylhexanol alcohols as biodiesel additive in a CI
159 engine using a wave-shaped piston bowl geometry [32]. The alcohols were blended separately either with
160 rapeseed biodiesel or hydrotreated vegetable oil (HVO) at different volume fractions [32]. They reported that


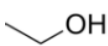

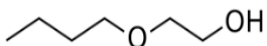
161 the CO and soot emissions were reduced when compared to fossil diesel [32]. The NO_x emission was increased,
 162 the least increase of NO_x emission was found to be 10% than fossil diesel for 2EH40H60 blend (40% 2-
 163 ethylhexanol and 60% HVO) at full load condition [32]. The 30% n-butanol and 70% HVO blend gave optimum
 164 engine performance when wave-shaped piston bowl geometry was used [32]. Radheshyam et al. assessed the
 165 impact of using 1-pentanol as fossil diesel additive at volume fractions of 5%, 10%, 20%, 30% and 40% [33].
 166 They reported that compared to pure fossil diesel operation and at high loads, 40% 1-pentanol blend gave 8%
 167 lower NO_x emission; however, the CO and HC emissions were increased from 0.01 % (vol.) to 0.04 % (vol.),
 168 and from 2.5 ppm to 11.5 ppm [33].

169 The above studies demonstrated that in general, blending biodiesel with alcohols improved engine performance
 170 characteristics. However, in the case of emission characteristics, no specific conclusions could be reached on
 171 whether adding alcohol helped to decrease the harmful gas emissions or not. So far the effects of ethanol,
 172 methanol and butanol on biodiesel fuelled engine operation were found in the literature. In this study, a new
 173 oxygenated additive '2-Butoxyethanol' will be used to assess the performance and emission characteristics of
 174 the engine operated with biodiesel-butoxyethanol blends. The '2-butoxyethanol' is an ether compound with
 175 ethanol branch containing additional oxygen molecule (Table 1). It is not a naturally occurring compound but
 176 obtained via different techniques in the laboratory environment like ethoxilation and etherification of butanol
 177 [34,35] Additional oxygen content in 2-butoxyethanol would further help to combust the biodiesel fuels more
 178 efficiently. Furthermore, the flash point of the 2-butoxyethanol is close to fossil diesel and higher than other
 179 alcohols used previously by the researchers (Table 1). In addition, 2-butoxyethanol have better surfactant
 180 properties which may help to reduce the corrosion rate of a biodiesel fuel on various engine components [34].
 181 Due to these promising fuel properties, investigation of the 2-butoxyethanol as a biodiesel additive will be
 182 carried out in this study. It is important to note that no such study was found in the literature. Two different
 183 biodiesels produced from waste cooking oil (WCO) and rapeseed oil (RO) will be used in this study. Biodiesels
 184 will be blended separately with 2-butoxyethanol. A 3-cylinder diesel engine will be used to test the fuels.
 185 BOSCH emission analyser and Kistler combustion analysis kit 'KiBox' will be used for measurements of
 186 emission gases and combustion parameters. The main objectives of the study are: (i) Production of waste
 187 cooking oil and rape seed oil biodiesels in the laboratory, (ii) Preparation of 2-Butoxyethanol - biodiesel blends
 188 and investigation of the fuel properties, (iii) To study the performance, combustion and emission characteristics
 189 of the multi-cylinder engine operated with 2-Butoxyethanol-biodiesel blends, and (iv) Comparison of the
 190 biodiesel-additive fuelled engine characteristics with neat biodiesels and neat fossil diesel operation. Physical
 191 and chemical properties of the biodiesels, biodiesel blends and fossil diesel fuel samples will be carried out
 192 according to international standards.

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195 **Table 1**
 196 Properties of common alcohols and 2-butoxyethanol.

	Methanol [36]	Ethanol [37]	Butanol [38]	2-butoxyethanol [39,40]
Structure				
Linear formula	CH ₃ OH	CH ₃ CH ₂ OH	CH ₃ (CH ₂) ₃ OH	CH ₃ (CH ₂) ₃ OCH ₂ CH ₂ OH
Molecular weight (g/mol)	32.042	46.069	74.123	118.176
Heat of vaporisation (kJ/mol at 25 °C)	37.34	42.32	52.35	56.59
Miscibility with organic solvents	Yes	Yes	Yes	Yes
Kinematic viscosity (at 25 °C, mm ² /s)	0.69	1.36	3.14	3.15
Density (kg/m ³)	792	789	810	900
Flash point (°C)	12	17	29	62
Boiling point (°C)	64.7	79	117.6	171
Melting point (°C)	-98	-117	-90	-75

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2. Materials and methods

2.1 Biodiesels production

Two biodiesels were produced in the laboratory using two different feedstock ie. waste cooking oil and rapeseed oil. Waste cooking oil was collected from a local restaurant in Birmingham and rapeseed oil was procured from a supermarket. The feedstock was first filtered using sock filter, and then transesterified using methanol and potassium hydroxide (KOH) catalyst. Initially, feedstock was heated up to approximately 55°C temperature. Then a mixture of methanol and KOH was introduced into the heated feedstock. Methanol to oil ratio was 1:5 by volume. The amount of KOH required was calculated by titration method. The mixture was stirred mechanically for around 30 minutes and transferred into a separator funnel for phase separation. The mixture was kept in the lab undisturbed for 24 hours, after that glycerol was removed and pure biodiesels were collected. Finally, produced biodiesels were washed by spraying distilled water. The water was removed from the biodiesel by separation technique and the washing was repeated couple of times until a clear colour biodiesel was obtained. Figure 1 shows the reaction schematic of the transesterification process. One (1) mole of triglyceride (feedstock) reacted with three (3) moles of methanol in the presence of KOH catalyst. The product is a mixture of glycerol and fatty acid methyl esters.

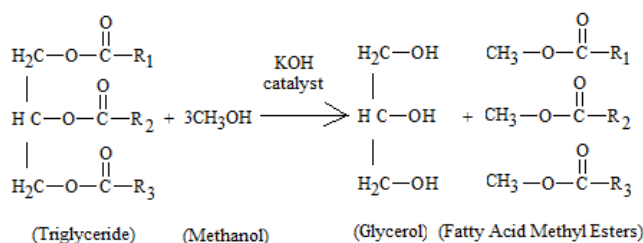


Fig. 1. Transesterification reaction mechanism

2.2 Alcohol blends preparation and fuel characterisation

2.2.1 Additive mixing and characterisation

2-Butoxyethanol (99% purity) was purchased from Fisher Scientific (UK) and used as a biodiesel additive in the current study. The amount of additive added to biodiesel was 15% (by volume); five different fuel samples were prepared: Ultra-low Sulphur Diesel (ULSD) as a reference fuel, neat waste cooking oil biodiesel (W100), blend of 85% waste cooking oil biodiesel and 15% of 2-butoxyethanol (W85), neat rapeseed oil biodiesel (R100), blend of 85% rapeseed oil biodiesel and 15% of 2-butoxyethanol (R85) (see Figure 2). The 2-butoxyethanol additive was miscible with biodiesels, no phase separation or solid formation was observed. Thus, no surfactant or mechanical stirring was needed. The reference ULSD diesel was purchased from Esso UK which satisfy the BS EN 590 specification [41]. The physical and chemical properties of the fuel samples were measured at the mechanical and chemical engineering laboratories of Aston University (Birmingham, UK). The calorific values were measured by bomb calorimeter (model Parr 6100) having an accuracy of ± 0.1%. Kinematic viscosities were measured (according to ASTM D 445 and ISO 3105 standards) using the Cannon-Fenske viscometer (M100) and thermostatic water bath; the measurement uncertainty was 0.16%. The density was measured by a hydrometer according to ASTM D7544 standard. Stanhope-Seta closed cup flash point tester (model: Setaflash 33000-0) was used to measure the flash point temperatures of the samples with the accuracy of ±0.5.



Fig. 2. Fuel samples from left to right: fossil diesel, WCO, W100, W85, rapeseed oil, R100 and R85

2.2.2 Gas chromatography and mass spectrum analyses

The fatty acid methyl ester (FAME) contents of the biodiesel were determined by the gas chromatography Thermo Trace 1300 coupled with mass spectrometer (GCMS) equipment. Separation was performed on a capillary column Elite-5MS (30 m × 0.22 mm, 0.25 μm). The carrier gas was Helium with flow rate of 1.25 mL/min. The column temperature was programmed from 100 to 275 °C at the rate of 10 °C/min. Fuel sample of 0.05 g was dissolved in 50 ml of methanol, the mixture was then placed into ultrasonicator for 15 minutes. Then, 0.1 μL of the prepared sample was transferred into test tube and loaded to the GCMS equipment. A split mode was used with the split ratio of 1:10. The temperature of the injector was set at 280 °C. The mass spectrometer was set to scan in the range of 50–600 m/z with electron impact (EI) mode of ionization, the MS transfer line and the ion source temperatures were set at 250 °C and 200 °C, respectively. The Carbon Hydrogen Oxygen (CHO) analysis, iodine value and cetane number of the fuels were estimated from the FAME composition found by GCMS analysis. Mass percentages/fractions of FAME components were multiplied by the relative values found in the literature (Table 2) to estimate the iodine value, cetane number and CHO content (equations 1 and 2).

$$Iodine\ Value_{Fuel} = \sum (Percent\ FAME_i \times Factor\ FAME_i) \quad (1)$$

$$Cetane\ Number_{Fuel} = \sum (Fraction\ FAME_i \times Cetane\ Number\ FAME_i) \quad (2)$$

Table 2

Fuel properties of individual FAME compounds.

FAME		Iodine value [42]	Cetane number [43]	Cetane number [44]	Carbon [45]	Hydrogen [45]	Oxygen [45]
Myristic	C14:0	0	66.2	65.4	0.74	0.12	0.1322
Palmitic	C16:0	0	74.3	73.9	0.76	0.13	0.1185
Palmitoleic	C16:1	0.95	51	53.3	0.76	0.12	0.1194
Stearic	C18:0	0	75.6	82.3	0.77	0.13	0.1074
Oleic	C18:1	0.86	56.5	61.7	0.77	0.12	0.1081
Linoleic	C18:2	1.732	38.2	41.1	0.78	0.12	0.1088
Linolenic	C18:3	2.616	22.7	20.5	0.78	0.11	0.1096
Arachidic	C20:0	0	100	90.8	0.77	0.13	0.0982
gadoleic	C20:1	0.785	64.8	70.2	0.78	0.12	0.0988
Behenic	C22:0	0	100	100	0.78	0.13	0.0904
Erucic	C22:1	0.723	76	78.7	0.78	0.13	0.0909

2.3 Engine test rig and instrument

In this research, three-cylinder Lister Petter compression ignition engine having an indirect injection system was used. Table 3 shows technical specification of the engine. The engine speed was kept constant at the rated speed of 1500 rpm throughout the experiments. Approximately an hour engine tests were conducted to test each samples ie. W100, W85, R100, R85 and fossil diesel. Engine operating conditions such as air intake system, tail pipe configuration, lubricant, cooling agent, compression ratio, break mean effective pressure etc. were kept identical for each test. Engine performance, combustion and exhaust gas emission parameters were collected at six different engine loads: around 20%, 40%, 60%, 70%, 80%, and 100%. In order to get correct readings, the engine was allowed to run around 20 minutes between fuel changes. The tests procedures followed were: (i) the engine was first started with fossil diesel, (ii) then switched to neat biodiesel, and (iii) then switched to biodiesel-additive blend operation. In addition, the fuel supply system was flashed with the diesel by running the engine on diesel about 40 minutes before changing from WCO biodiesel fuels to RO biodiesel fuels. During the measurements, multiple readings were recorded in order to minimise possible errors and to ensure repeatability of the observed data. Figure 3 illustrates the experimental setup used in this study. The test engine was equipped with a dual fuel supply system which can be operated manually by a T-junction valve. At the end of the test, the

280 engine was switched back to fossil diesel and operated for about 40 minutes to flush off the fuel supply and
 281 injection systems. An eddy current (Froude Hofmann AG80HS) dynamometer, with ± 1 rpm speed and ± 0.4 Nm
 282 torque accuracies was used. Fuel consumption of the engine was measured manually using a graduated cylinder
 283 on the fuel supply line. A commercial (Bosh BEA 850) five-gas emission analyser was used for measuring the
 284 tailpipe emissions. By this device, it was possible to measure the exhaust gases like HC, CO, CO₂, O₂, NO and
 285 excess air ratio (λ). Furthermore, the smoke intensity of the exhaust gas was analysed through the Bosch
 286 RTM 430 smoke opacity measurement instrument. The combustion parameters of the test fuels were collected
 287 through pressure sensor installed inside the first cylinder (close to radiator) of the engine. Kistler 6125C11
 288 pressure sensor with the Kistler 5064B11 charge amplifier was installed for the measurement of in-cylinder
 289 pressure. To log the fuel injection pressures, Kister 4065A500A0 pressure sensor along with the Kister 4618A0
 290 amplifier was used. Crank angle was detected by using the Kister 2614A optical encoder. The Kister product,
 291 2893AK8 model KiBox was installed to the system to log the data. The KiBoxCockpit software (supplied by
 292 Kistler) was connected to the KiBox hardware through an ethernet connection for monitoring and analysing the
 293 combustion parameters.

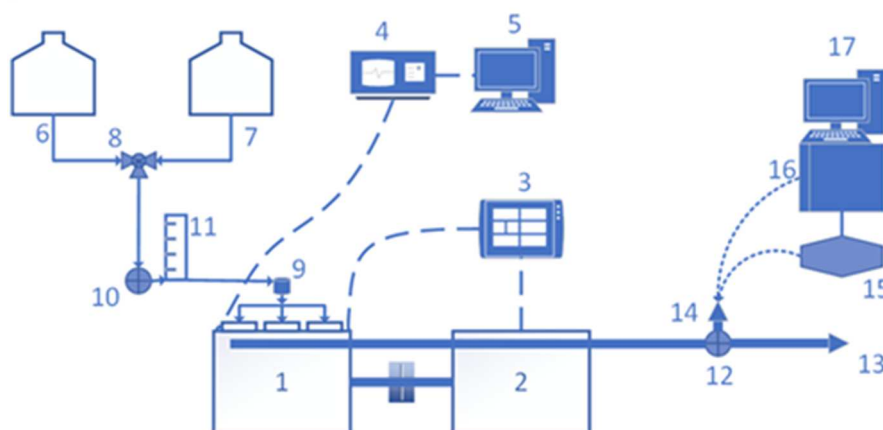
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295 **Table 3**
 296 Technical specification of the engine.

Manufacturer	Lister Petter (UK)
Model	LPWS Bio3 water cooled
Cylinder number	3
Exhaust gas recirculation	0%
Rated speed	1500 rpm
Continuous power at rated speed	9.9 kW
Fuel injection type	Indirect injection. Self-vent fuel system with individual fuel injection pumps
Fuel pump injection timing	20 ° BTDC
Aspiration	Naturally aspired
Cylinder capacity	1.395 L
Compression ratio	1:22
Continuous power fuel consumption at 1500 rpm	3.19 L/hr (fossil diesel)
Exhaust gas flow	41.4 L/sec at full loads at 1500 rpm
Jacket water flow at full load	33 L/min (at 1500 rpm)

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Fig. 3. Schematic of the engine test rig.

301 [1 engine; 2 dynamometer; 3 dynamometer controller; 4 Kister combustion analyser; 5 computer to collect & visualise combustion data; 6
 302 fossil diesel tank; 7 biodiesel tank; 8 three-way valve; 9 fuel filter; 10 valve; 11 graduated cylinder to measure fuel consumption; 12 valve
 303 on the exhaust line; 13 exhaust gas exit; 14 branch on the exhaust line to measure emissions; 15 smoke opacity unit; 16 Data acquisition for
 304 smoke meter and exhaust gas analyser; 17 computer to collect & visualise exhaust gas emissions].

2.4 Error analysis

The error analysis is important for experimental studies. There are many factors that can cause uncertainties and errors in any experimental study such as environmental conditions, equipment selection and instrument calibration [33]. This error analysis helps to quantify the overall accuracy of the experimental investigation. Knowing the uncertainties of the exhaust gas analyser, dynamometer and the combustion analyser, specific uncertainties for BSFC, BTE, speed, load, time, crank angle, in-cylinder pressure and exhaust emissions were calculated by partial differentiation method (Table 4). This method was used for similar type of studies [33]. Specific uncertainties of the each parameter were calculated by minimum of 5 consecutive readings and overall uncertainty was calculated using equation 3.

$$Uncertainty = \sqrt{\sum (specific\ uncertainties)^2} = \pm 2.040\% \quad (3)$$

Table 4

The uncertainties of various parameters.

Measurements	Uncertainty (%)	Measurements	Uncertainty (%)
BSFC	0.8	CO ₂	0.1
BTE	0.8	O ₂	0.1
Speed	0.2	HC	0.9
Load	0.2	CO ₂	0.1
Time	0.8	NO	0.1
Crank angle	0.1	smoke	0.9
Cylinder pressure	0.7		

3. Results and discussion

In this section, fuel properties, engine performance, combustion characteristics, exhaust gas emissions and cost analysis of the test fuels are presented. The effects of 2-butoxyethanol additive on biodiesels are discussed, the results are compared with the corresponding results of the fossil diesel and neat biodiesels (W100 and R100).

3.1 Fuel properties

The FAME compositions of the biodiesels with and without 2-butoxyethanol additive are shown in Table 5. The major FAMES found in this study were C16:0, C18:0, C18:1 and C18:2. Peaks for the mentioned FAMES were clearly observed on the mass spectra and presented in Figure 4. According to GCMS results, for all biodiesels (including blends with 2-butoxyethanol), the first peaks were obtained at retention time of around 18 minutes which were representing the presence of the C16:0 (Figure 4 a, b, c and d). On the other hand, the following peaks between 21 and 22 minutes were accounted for C18 group FAMES such as C18:0, C18:1 and C18:2. It was clearly observed that 2-butoxyethanol additive effected the mass fractions of the C18:1 and C18:2 FAMES in the neat biodiesels by about 3% in W100 and 6% in R100. This phenomena directly influences the fuel properties especially cetane number and iodine value. According to BS EN 14214 standard for biodiesel, iodine value of biodiesel is directly proportional to FAME breakdown of the biodiesel [42]. Similarly, other fuel properties such as cetane number, lower heating value (LHV), density, cloud point etc. could also be predicted through FAME composition [44] (Table 2).

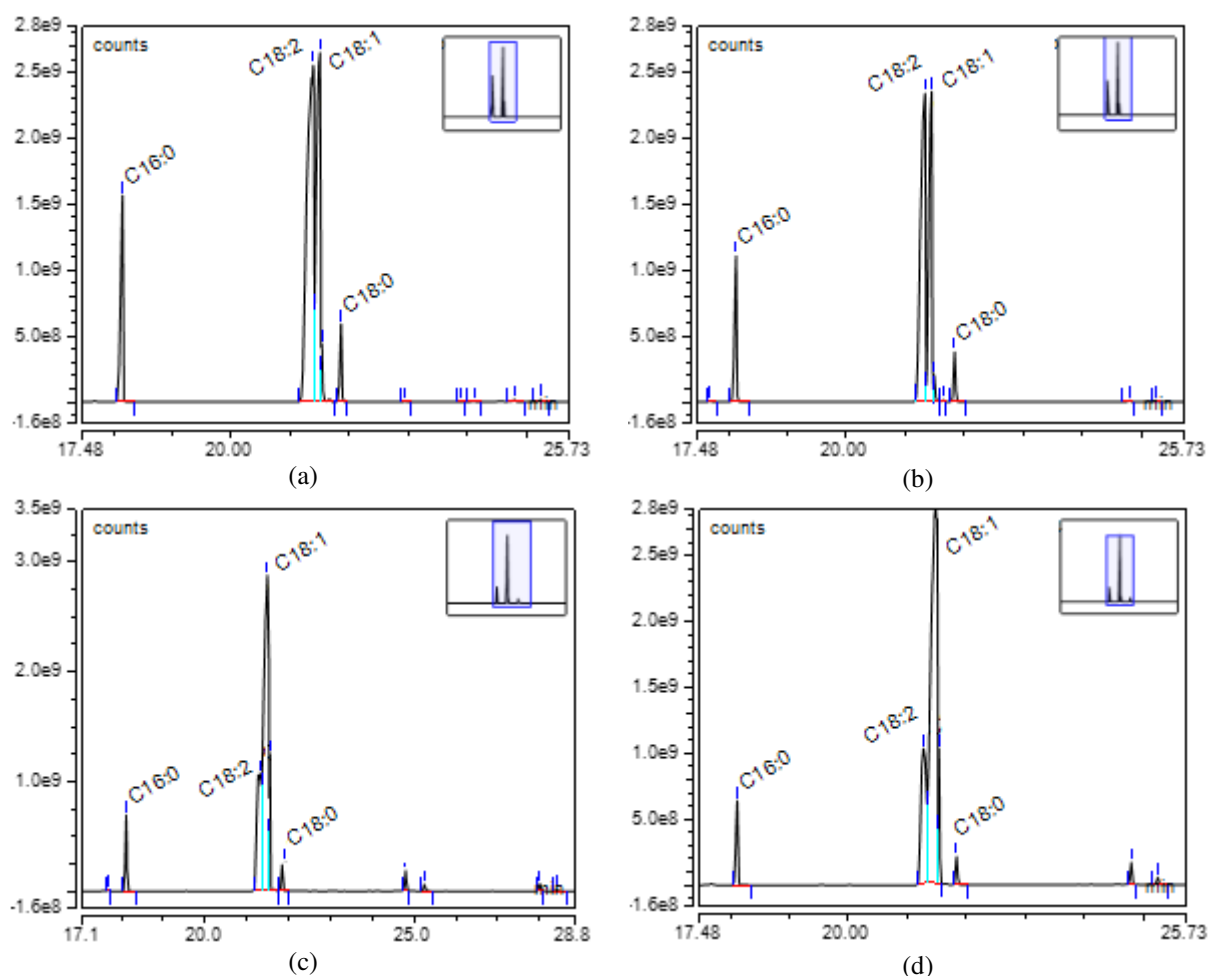


Fig. 4. Gas chromatography and mass spectrum analysis of (a) W100, (b) W85, (c) R100 and (d) R85.

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Table 5

345 Mass percentages of the measured fatty acid methyl esters in biodiesels/blends.
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FAME			Biodiesels/Blends			
Formula	Fatty acid	Designation	W100	W85	R100	R85
$C_{17}H_{34}O_2$	Palmitic	C16:0	10.4	10.1	4.1	4.3
$C_{17}H_{32}O_2$	Palmitoleic	C16:1	0.0	0.1	0.1	0.0
$C_{19}H_{38}O_2$	Stearic	C18:0	3.3	3.4	1.5	1.6
$C_{19}H_{36}O_2$	Oleic	C18:1	52.9	50	65.8	72.3
$C_{19}H_{34}O_2$	Linoleic	C18:2	32.8	36.0	26.0	19.2
$C_{19}H_{32}O_2$	Linolenic	C18:3	0.0	0.1	0.0	0.0
$C_{21}H_{42}O_2$	Arachidic	C20:0	0.2	0.0	0.5	0.5
$C_{21}H_{40}O_2$	gadoleic	C20:1	0.2	0.4	1.3	1.4
$C_{23}H_{46}O_2$	Behenic	C22:0	0.2	0.0	0.2	0.2
$C_{23}H_{44}O_2$	Erucic	C22:1	0.0	0.0	0.5	0.5

347

348

349 Table 6 shows the fuel properties of the test fuels and the British biodiesel norms ie. BS EN 14 214. The
350 kinematic viscosities (at 40 °C) of the W100 and R100 biodiesels were reduced by 12.5% and 9.8% respectively
351 when 15% (by volume) 2-butoxyethanol additive was added to biodiesels. The densities of the W100 and R100
352 biodiesels did not change with the addition of the additive, as 2-butoxyethanol has similar density value like
353 biodiesels (Table 1). However, the higher heating value (HHV) and flash point temperatures were negatively
354 affected by the 2-butoxyethanol additive. Due to the additive, the HHV of the W100 and R100 were reduced by

355 about 1% and 1.8% respectively. Similarly, the flash points of W85 and R85 were measured relatively low as 87
 356 °C (decreased by about 49% than W100) and 81 °C (decreased by about 53% than R100). This requires more
 357 precautions for storage and transportation of the W85 and R85 fuels. Iodine value and degree of unsaturation
 358 were also slightly reduced due to the additive addition. Carbon, hydrogen and oxygen contents were not
 359 significantly affected by the 2-butoxyethanol additive (Table 6). The cetane number was slightly improved when
 360 2-butoxyethanol was added to biodiesel (Table 6). Overall, fuel characterisation results proved that 2-
 361 butoxyethanol (by 15% volume) can be used as biodiesel additive to replace neat biodiesel or neat fossil diesel
 362 use in the compression ignition (CI) engine.

363

364 **Table 6**
 365 Fuel properties of the test fuels and BS EN 14214 standard.

Fuel Property	Unit	Method	Diesel	W100	W85	R100	R85	BS EN 14214
Kinematic Viscosity at 40°C	(mm ² /s)	EN ISO 3104	2.78	5.05	4.42	4.6	4.15	3.5-5.0
Kinematic Viscosity at 20°C	(mm ² /s)	EN ISO 3104	4.39	7.61	6.66	6.69	6.21	n/a
Density	(kg/m ³)	EN ISO 3675	828	882	882	880	880	860-900
HHV	(MJ/kg)	Bomb calorimeter	45.16	38.4	38	39.2	38.5	n/a
LHV	(MJ/kg)	Theoretical	41.99	35.71	35.34	36.46	35.81	n/a
Flash point	(°C)	EN ISO 3679	61.5	169	87	173	81	101 min
Iodine value	(g iodine/100 g)	EN 14111	n/a	120	118	103	97	120 max
Linolenic acid methyl ester	(% m/m)	EN 14103	n/a	0	0	0	0	12
Cetane number	(-)	Calculated[44]	54	53	53	58	59	51 min
Cetane number	(-)	Calculated[43]	54	49	50	53	55	51 min
Degree of unsaturation	(% m/m)	Calculated[46]	n/a	2.39	2.37	2.20	2.13	n/a
Carbon content	(% m/m)	Theoretical[45]	86.6	77.14	77.13	77.12	77.08	n/a
Hydrogen content	(% m/m)	Theoretical[45]	13.4	11.91	11.93	12.04	12.08	n/a
Oxygen content	(% m/m)	Theoretical[45]	0.07	10.95	10.95	10.84	10.84	n/a

366

367

368 3.2 Engine performance

369

370 The biodiesel-additive blends gave higher BSFC than both neat biodiesels and fossil diesel (Figure 5). On
 371 average, BSFC of the W85 was 4.3% and 14.1% higher than W100 and diesel fuel respectively. Similarly,
 372 BSFC of the R85 was observed as 5.2% and 18.8% greater than R100 and diesel respectively. This increase on
 373 BSFC can be attributed to the reduced LHV of the blends (due to addition of additive) (Table 6). However, it
 374 was found out that the BSFC of the biodiesel blends were improved with the increase in engine load. At
 375 maximum load, the BSFC of the biodiesel blends were only 1% higher than neat biodiesels. This was mainly
 376 due to the higher enthalpy of vaporisation of the blends, which led to better combustion under higher engine
 377 loads (ie. temperatures) [26]. Both W85 and R85 fuels produced similar BSFC trends; however, BSFC of W85
 378 fuel was slightly (0-3%) lower than that of R85 fuel (Figure 5). Figure 6 shows the relationship between the
 379 brake Thermal Efficiency (BTE) and engine load for all test fuels. Compared to neat biodiesels, the BTE of the
 380 engine was observed 3-6% lower for W85 and R85 fuels. However, the results showed that of all the test fuels,
 381 W100 and W85 fuels gave highest BTE. The BTE of the W100 and W85 fuels were approximately 5% and 3%
 382 higher than the corresponding fossil diesel values. The improved BTE's can be explained by the higher oxygen
 383 content of the biodiesels which in turn enhances the combustion [47,48]. Despite the fact that the HHV of W100
 384 and W85 were lower than fossil diesel, the presence of fuel borne oxygen content improved the diffusion
 385 combustion, which resulted higher BTE [49]. On the other hand, R85 fuel provided slightly lower BTE than the
 386 fossil diesel. The BTE of the R100 fuel was around 4% lower than that of W100. These differences in BTE
 387 values between two different biodiesels could be attributed to their fuel properties such as oxygen content,
 388 density and iodine value (Table 6).

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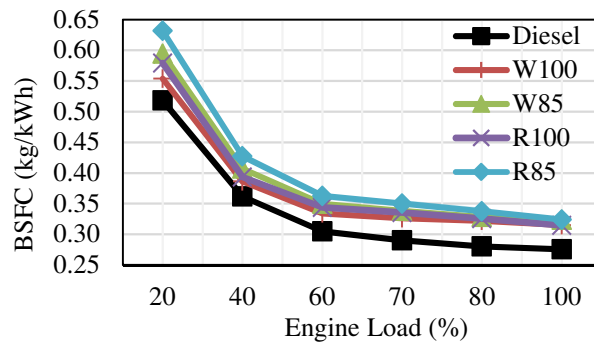


Fig. 5. BSFC of test fuels as a function of the engine loads.

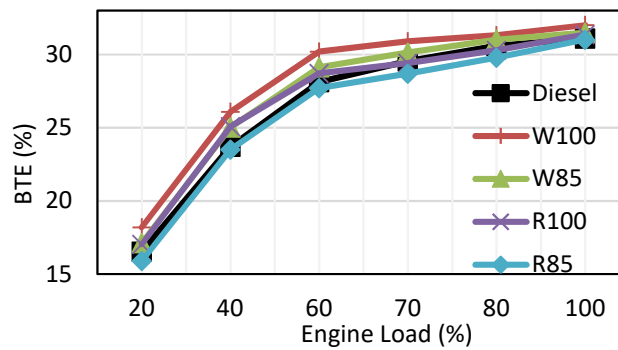
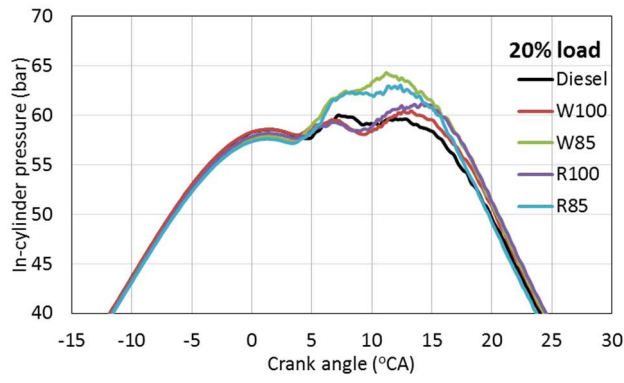


Fig. 6. BTE of test fuels as a function of engine loads.

3.3 Combustion characteristics

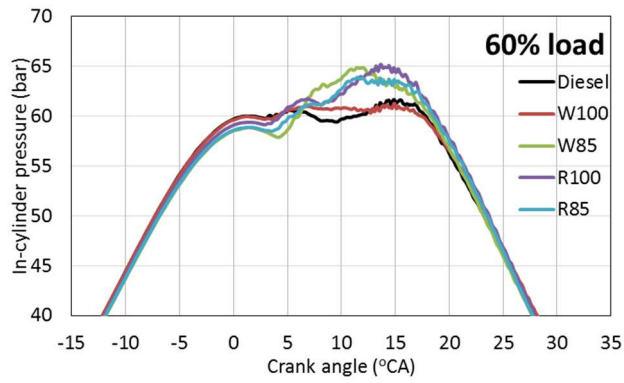
Combustion parameters data such as total heat release, heat release rate, in-cylinder pressure, combustion start and finish times, total combustion duration, fuel injection pressure and knock intensity were recorded and analysed. In-cylinder pressure and heat release data were presented (using 51 cycles) with respect to the crank angle position. Whereas, rest of the combustion parameters were illustrated with respect to the engine load, the arithmetic average of 51 indication cycles were used. Engine was stable with all fuels including biodiesel-additive blends. Figure 7 represents in-cylinder pressure behaviour of the test fuels at low, mid-range, and high loads. At the lowest load (20%), in-cylinder pressures of the neat biodiesels (W100 and R100) were quite similar to those obtained for fossil diesel. Whereas, the peak in-cylinder pressures at lowest load were found to be approximately 6% higher for W85 and R85 fuels (Figure 7a). The higher values of the peak in-cylinder pressures were caused due to the increased volatility of the biodiesel blends. The results also indicated that as the engine load increases, the in-cylinder pressures of the neat biodiesels were also increased almost at a similar rate with the biodiesel blends. For example, at 60% engine load, R100 and R85 fuels provided similar peak in-cylinder pressure; however, they are approximately 7.7% higher than the corresponding value of fossil diesel (Figure 7b). Increased in-cylinder pressures observed for biodiesels and their blends proved that combustion was improved due to the presence of higher oxygen content in those fuels. At full load condition, all biofuels gave about 6% higher peak pressures than the corresponding value obtained for fossil diesel (Figure 7d). At full load, peak in-cylinder pressure of all biodiesels (and blends) was delayed by about 5 °CA when compared to fossil diesel (Figure 7d). This was caused due to the relatively higher ignition delays of the biodiesels and their blends than the corresponding value of fossil diesel.



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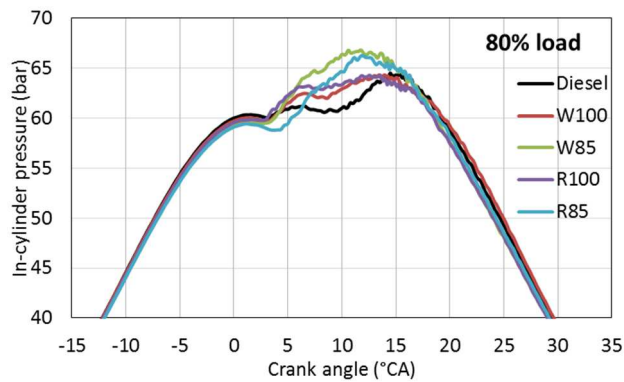
(a)



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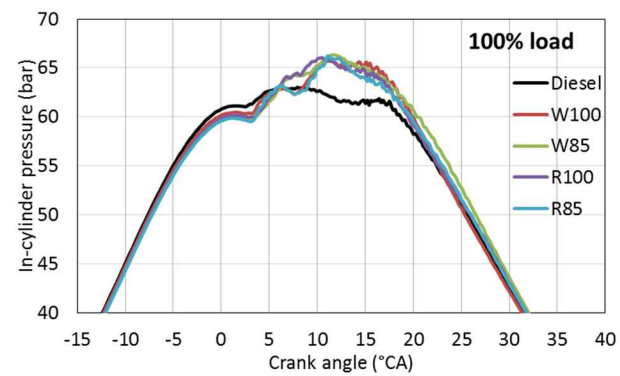
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(c)



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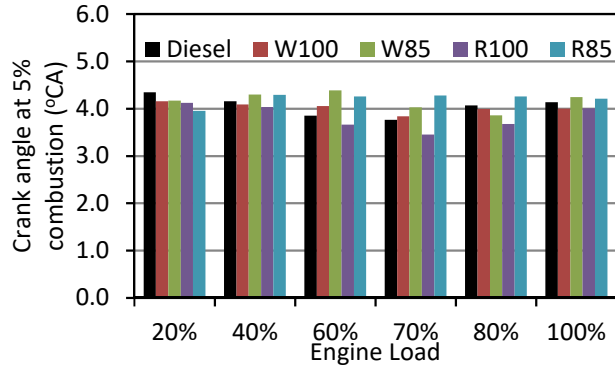
(d)

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Fig. 7. In-cylinder pressure and crank angles at (a) 20% (b) 60% (c) 80% and (d) 100% loads.

427 Start and end of combustion were analysed and presented in Figure 8. Combustion start angle was measured
 428 when 5% of the combustion took place and similarly combustion finish angle was recorded at 90% of the total
 429 combustion (Figure 8a and 8b). The differences between the finish and start angles were reported to identify the
 430 total combustion duration (Figure 8c). In most engine loads, start of combustion of biodiesel-additive blends
 431 were earlier than fossil diesel (Figure 8a). However, it was found that end of combustion for biodiesel-additive
 432 blends occurred earlier than fossil diesel and neat biodiesels (Figure 8b). These results agree with the similar
 433 studies (with different alcohol blends) found in the literature [24,49].

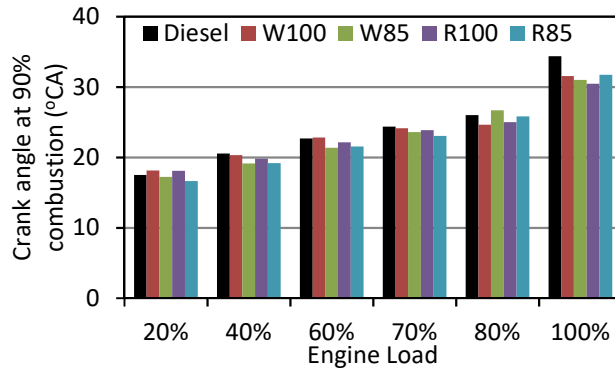
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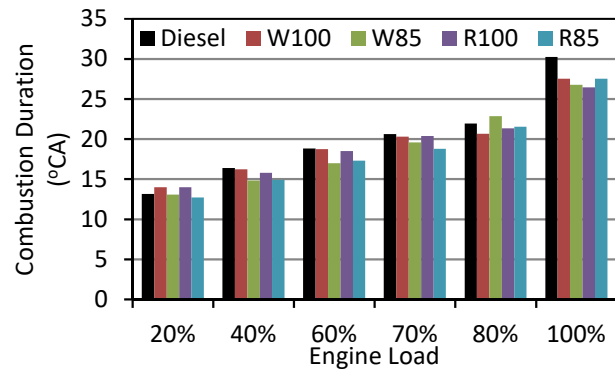
(a)



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(b)



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(c)

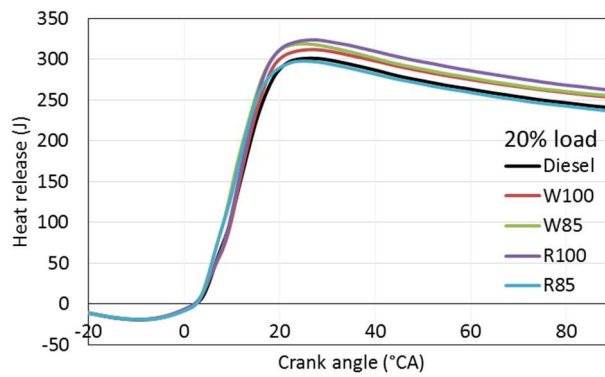
441 **Fig. 8.** Combustion characteristics: (a) start of combustion, (b) end of combustion, and (c) combustion duration.

442

443 Total combustion duration of the W85 fuel was approximately 0-4 °CA and 0-1 °CA lower than fossil diesel
 444 and W100 fuel respectively (except 80% load) – Figure 8c. Similarly, combustion duration of the R85 was

445 reported 1-2 °CA less than both diesel and R100 at low and mid-range loads. When compared to fossil diesel,
 446 maximum reductions in combustion duration were observed at the highest load by approximately 3 °CA, 4 °CA,
 447 4 °CA and 3 °CA for W100, W85, R100 and R85 respectively (Figure 8c). This analyses proved that once
 448 combustion starts, 2-butoxyethanol blends of biodiesels burn quicker than fossil diesel and neat biodiesels.
 449 Reduced viscosity and higher oxygen content in the biodiesel-additive blends might have caused this behaviour.
 450 Moreover, increased volatility and better dissociation of fuel molecules might have helped in rapid burning of
 451 the 2-butoxyethanol blends. Energy release data of all fuels are shown in Figure 9. W85 and R85 fuels were
 452 providing higher heat release especially during the early phases ie. between approximately 3 ° and 15 ° CA at all
 453 engine loads. For example, at the low (20%) and medium (60%) engine loads, heat release data of both W85 and
 454 R85 fuels at 10 °CA was about 17% (23 Joules) higher than the corresponding values of fossil diesel and neat
 455 biodiesels (Figure 9). The higher heat release of the biodiesel-additive blends (W85 and R85) can be attributed
 456 to their increased volatility and lower viscosity. On the other hand, it was found that at high load, due to the high
 457 combustion temperature, heat release of the blends and neat biodiesels were comparable (Figure 9d). Maximum
 458 heat release rates of the fuels were analysed for 51 cycles and the arithmetic mean is shown in Figure 10.
 459 Similar to heat release, no clear trend was observed for maximum heat release rates at low loads. However, it
 460 was seen that, after 60% engine load, the deviations in heat release rates between the biodiesels and their blends
 461 with additive were not significant. The first reason of this was believed to be relatively higher combustion
 462 temperature which eliminates the effect of high viscosities. Secondly, the higher enthalpy of vaporisation of 2-
 463 butoxyethanol resulted in achieving better maximum heat release rates at higher combustion temperatures.

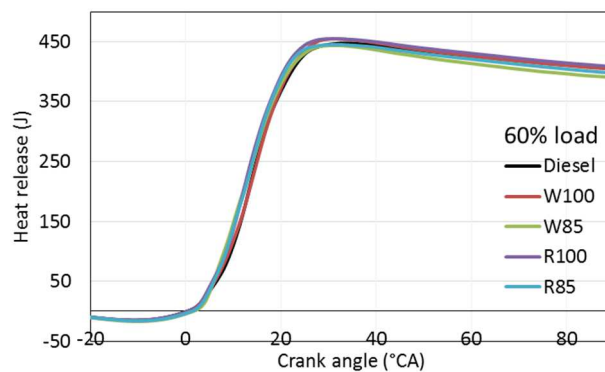
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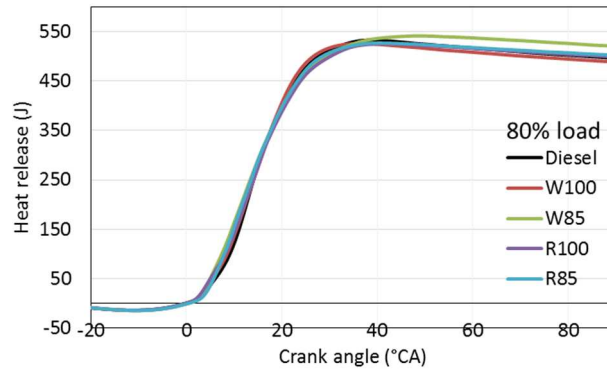
(a)



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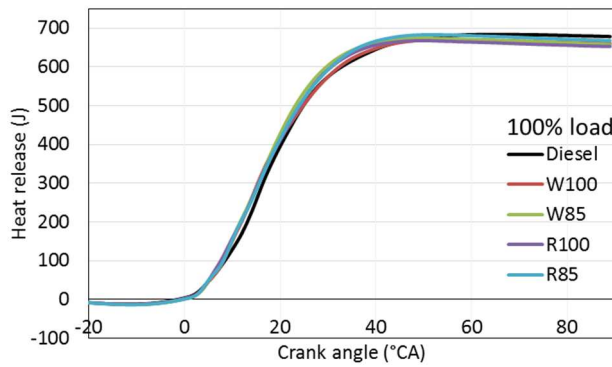
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(b)



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(c)

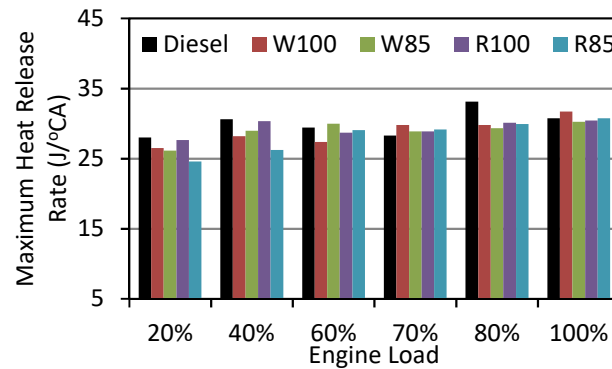


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(d)

Fig. 9. Heat release of the test fuels at various loads: (a) at 20%, (b) at 60%, (c) at 80%, and (d) at 100% loads.

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Fig. 10. Maximum heat release rates of the fuels at different engine loads.

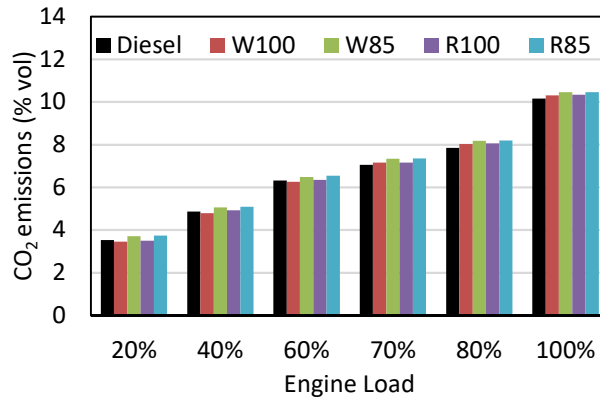
3.4 Exhaust gas emissions

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Figure 11 shows variation of CO₂ gas emissions with engine loads. It was observed that CO₂ gas emissions were increased with the increase in engine loads (Figure 11) as fuel consumption increases with the increase in engine load. Although, all test fuels exhibited comparable CO₂ emissions, biodiesel blends were emitting slightly higher (approximately 1-2%) CO₂ than other fuels. This slight increased may be due to the enhanced combustion of the 2-butoxyethanol blends which turns more carbon atoms into carbon dioxide. Unlike CO₂ emission, O₂ emissions were linearly decreasing with the increasing engine load (Figure 12). The amount of air intake is constant, and as a result, the O₂ gas emission decreases due to the increased reaction between the

487 relatively higher amount of fuel molecules and the same amount of air (oxygen) molecules at the higher loads.
 488 Theoretically, biodiesels are likely to reduce the HC emission as the additional oxygen content provides more
 489 complete combustion [50]. Hence, biodiesel blends were expected to emit reduced HC emission as total oxygen
 490 content increases with addition of 2-butoxyethanol additive. Experimental results proved the theory as W85 and
 491 R85 emitted almost up to 100% reduced HC emissions than both their neat biodiesel versions and the fossil
 492 diesel (Figure 13). However, R85 provided uneven HC emission distribution (Figure 13), this could be due to
 493 the error in measurement and accuracy level of the gas analyser.

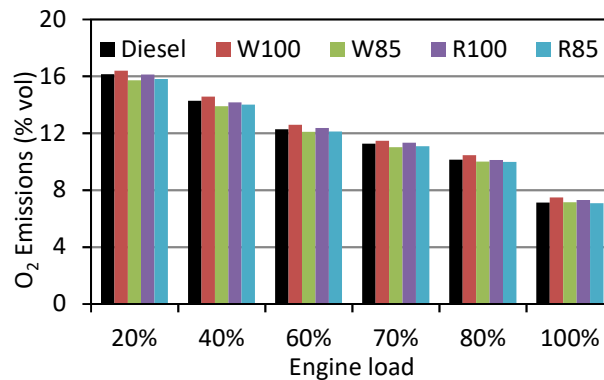
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496 **Fig. 11.** CO₂ emissions of the test fuels at different engine loads.

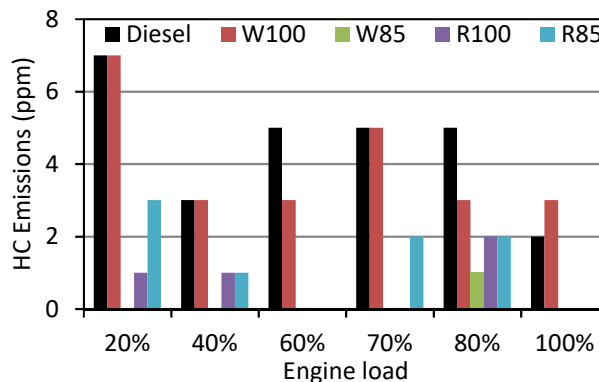
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499 **Fig. 12.** O₂ emissions of the test fuels at different engine loads.

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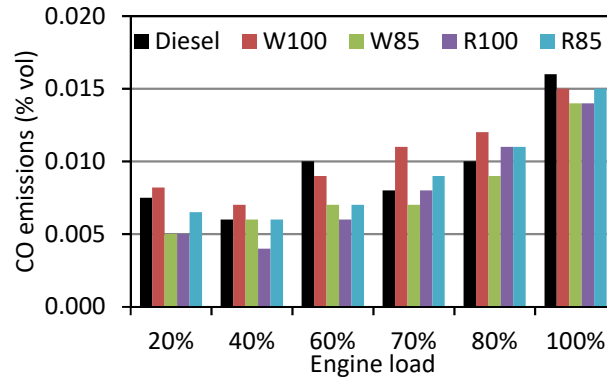


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502 **Fig. 13.** HC emissions of the test fuels at different engine loads.

503 Figure 14 provides the CO emissions of the test fuels at different loads. It can be clearly deemed that on
 504 average, addition of 2-butoxyethanol into WCO biodiesel decreased the CO emission by approximately 25%. In
 505 contrast, 2-butoxyethanol additive increased the CO emission by around 12% when added to RO biodiesel. This
 506 result shows that type of biodiesel feedstock is important for 2-butoxyethanol blending. Furthermore, W85
 507 emitted 10% less CO (on average) compared to fossil diesel. The reduction in CO emission was presumably due
 508 to relatively higher oxygen content (Table 6) and reduced viscosity of the WCO biodiesel which led to better
 509 combustion [51].

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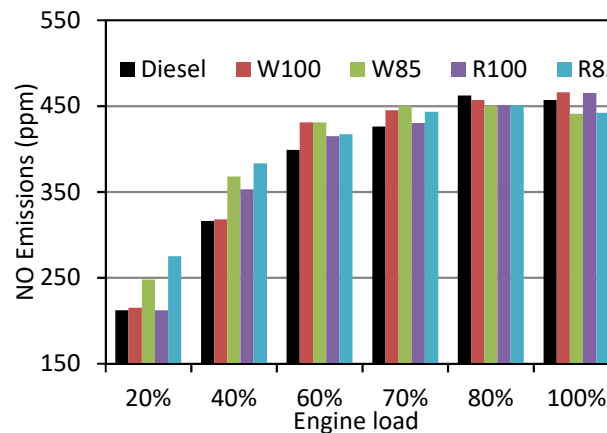
511

512 **Fig. 14.** CO emissions of the test fuels at different engine loads.

513

514 Emission of nitrogen oxide gas is shown in Figure 15. The 2-butoxyethanol blends exhibited different
 515 behaviours at low, medium and high loads. To illustrate, until the 40% engine load, W85 emitted around 15%
 516 higher NO emission than W100 fuel. Then at medium loads, NO emissions of W100 and W85 were comparable.
 517 At full load, W85 fuel gave about 5.4% and 3.5% lower NO emission than neat biodiesel and fossil diesel
 518 respectively. Figure 16 presents smoke opacity of the test fuels at various loads. It was clearly observed that
 519 smoke opacities of the biodiesels (and blends) were significantly reduced when the load on the engine was
 520 increased. Compared to fossil diesel, maximum reductions on smoke opacities were recorded at the highest
 521 engine load as 73%, 79%, 66% and 71% for W100, W85, R100 and R85 fuels respectively. Reductions in
 522 smoke opacities were attributed to the extra oxygen content present in biodiesels (and blends) [52]. At full load,
 523 the smoke opacity values of the biodiesel-additive blends were approximately 5% lower than the corresponding
 524 values found for neat biodiesels.

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527 **Fig. 15.** NO emissions as a function of engine load.

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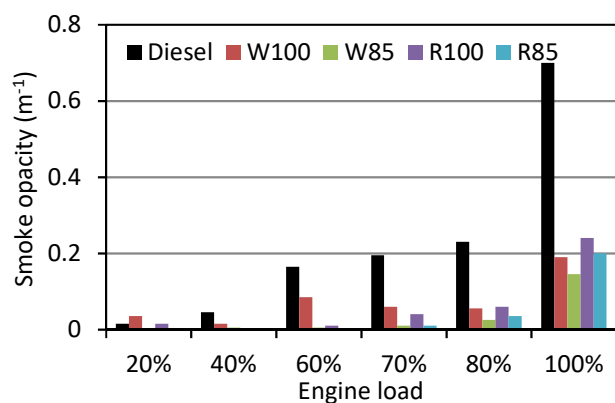


Fig. 16. Smoke opacity of the test fuels at different engine loads.

3.5 Economic feasibility analysis

A simple economic analysis was carried out to analyse the feasibility of using 2-butoxyethanol as biodiesel additive. Waste cooking oil was obtained from a restaurant in Birmingham, UK. Whereas, RO was bought from a commercial supplier. Table 7 shows list of materials with their quantity to prepare a litre of biodiesel and the biodiesel-additive blends. Note that, materials used for titration purposes such as isopropyl alcohol and indicator were not included in the analysis. In addition, it was assumed that the electrical power consumptions for heating and mechanical stirring were negligible. According to the data provided by the Department for Business, Energy & Industrial Strategy [53], diesel price in the UK was 115.63 pence/litre (including tax) on 3 July 2017. Table 8 shows the total cost of fuel samples, W100 and W85 fuels were approximately 100 and 35 pence/litre cheaper than the commercial fossil diesel. In addition, the cost of R100 was found to be equal to that of fossil diesel. However, the cost of the R85 was around 55 pence/litre higher than the diesel due to its feedstock price (Table 7).

Table 7
Quantity and the price of materials used to produce 1 litre of test fuel.

Substance	Quantity required to produce 1 L biodiesel	Quantity required to produce 1L 85%biodiesel-15%alcohol blend	Unit Price
WCO	1 L	0.85 L	0
RO	1 L	0.85 L	1 £/ L
Methanol	0.2 L	0.17 L	0.7 £/ L
KOH for WCO	10.5 g	8.9 g	1.5 £/kg
KOH for RO	8.2 g	7.0 g	1.5 £/kg
2-Butoxyethanol	0	0.15 L	4.8 £/ L

Table 8
Total costs of one litre fuel samples.

	Cost of W100 £/ L	Cost of W85 £/ L	Cost of R100 £/ L	Cost of R85 £/ L
Feedstock (WCO or RO)	0	0	1	0.85
Methanol	0.14	0.12	0.14	0.12
KOH	0.02	0.01	0.01	0.01
2-Butoxyethanol	0	0.72	0	0.72
Total cost	0.16	0.85	1.15	1.70

4. Conclusion

The 2-butoxyethanol additive (15% by volume) was added separately to waste cooking oil biodiesel and rapeseed oil biodiesel. The physical and chemical properties of these blends were measured and compared to the corresponding properties of the neat biodiesels and fossil diesel fuels. The fuels were tested in a multi-cylinder compression ignition engine. Engine performance, combustion and emission characteristics of the 2-butoxyethanol-WCO biodiesel (W85) and the 2-butoxyethanol-RO biodiesel (R85) blends were compared to both neat biodiesels (W100 & R100) and fossil diesel. No instability or abnormalities were observed in the in-cylinder pressure diagrams; i.e. the engine ran smoothly when 2-butoxyethanol-biodiesel blend was used in the engine. Overall, 2-butoxyethanol additive gave improved emissions when used with both biodiesels. However, considering engine performance, emission reduction and cost parameters, it was found out that 2-butoxyethanol-WCO biodiesel blend was superior to the 2-butoxyethanol-RO biodiesel blend. The major findings of the study are summarised below:

(i) BSFC of the WCO biodiesel was increased by approximately 4.3% when blended with the 2-butoxyethanol additive. The BSFC of the R85 was observed as 5.2% and 18.8% greater than R100 and diesel respectively. The additive decreased BTE of the W100 fuel by about 2.6%. Nevertheless, BTE of the W85 fuel was still 3.7% higher than the diesel.

(ii) Both W85 and R85 fuels released around 17% higher energy at the early stages of the combustion. At 80% engine load, the maximum heat release of the W85 was approximately 6.5% and 4.8% greater than the W100 and diesel respectively. Total combustion duration of the W85 was 4 °CA shorter than the fossil diesel fuel on average.

(iv) The NO emission of the W100 fuel was comparable with the diesel at the maximum engine load. W85 fuel reduced the NO emission by 5.4% and 3.5% when compared to the corresponding values of the W100 and neat fossil diesel. Both W85 and R85 fuels emitted almost up to 100% reduced HC emissions than neat biodiesels and the fossil diesel. Compared to diesel, W85 fuel gave significant reductions in CO, HC and smoke emissions by 36%, 100% and 79% respectively.

(v) Basic economic analysis showed that a litre of W85 fuel was about 30 pence cheaper than the commercial fossil diesel.

This study concludes that the 2-butoxyethanol could be used as an effective and safe biodiesel additive. Current study proved that 2-butoxyethanol additive enhanced the fuel properties, and gave significant improvement in engine performance and emission when the additive was added to WCO biodiesel. However, it should be noted that depending on the source of biodiesel feedstock, 2-butoxyethanol-biodiesel blends can be more expensive than fossil diesel. Further techno-economic analyses using other biodiesels need to be carried out and recommended as a future work. Investigation on the effects of fossil diesel addition (as a third component) into the 2-butoxyethanol-biodiesel blend is another R & D topic.

Acknowledgments

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